

(19)



Europäisches Patentamt

European Patent Office

Office européen des brevets



(11)

EP 0 712 817 B1

(12)

EUROPEAN PATENT SPECIFICATION

(45) Date of publication and mention
of the grant of the patent:
06.05.1999 Bulletin 1999/18

(51) Int. Cl.⁶: **C04B 28/04**, C04B 38/10,
E21B 33/13, E21B 33/138
// (C04B28/04, 24:12, 24:16,
24:32)

(21) Application number: **95308190.8**

(22) Date of filing: **15.11.1995**

(54) Method for cementing a conductor pipe in an underwater well

Verfahren zur Zementierung eines Führungsrohres in einem Unterwasserbohrloch

Méthode de cimentation d'un tube conducteur dans un puits sous-marin

(84) Designated Contracting States:
DE FR GB IT NL

(30) Priority: **21.11.1994 US 343058**

(43) Date of publication of application:
22.05.1996 Bulletin 1996/21

(73) Proprietor:
Halliburton Energy Services, Inc.
Duncan, Oklahoma 73536 (US)

(72) Inventor: **Griffith, James E.**
Loco, Oklahoma 73442 (US)

(74) Representative:
Wain, Christopher Paul et al
A.A. THORNTON & CO.
Northumberland House
303-306 High Holborn
London WC1V 7LE (GB)

(56) References cited:
EP-A- 0 449 360 **EP-A- 0 592 217**
FR-A- 2 680 781 **US-A- 5 133 409**
US-A- 5 213 161

• **PATENT ABSTRACTS OF JAPAN vol. 016 no. 411**
(C-0979), 31 August 1992 & JP-A-04 139080 (SK
KAKEN CO LTD) 13 May 1992,

Note: Within nine months from the publication of the mention of the grant of the European patent, any person may give notice to the European Patent Office of opposition to the European patent granted. Notice of opposition shall be filed in a written reasoned statement. It shall not be deemed to have been filed until the opposition fee has been paid. (Art. 99(1) European Patent Convention).

EP 0 712 817 B1

Description

[0001] This invention relates to a method of cementing a conductor pipe in an underwater well and is particularly (but not exclusively) useful in wells in water over 305m (1000 feet) deep where the surface mud is not well consolidated.

[0002] Well completions in water over 305m (1000 feet) deep often require special techniques to install conductor casing. Well completions at depths in excess of 610m (2000 feet) of water are often referred to as "deepwater" operations. In deepwater operations, the formations where conductor pipe is cemented that is less than 610m (2000 feet) below mud line (BML) are generally young geologically and are not well consolidated. The formations generally are the product of erosion from the continental shelf. This can cause two problems in cementing. The formation may be so weak that it may fracture during cementing and cause the loss of cement into the formation. Alternatively, the formation may experience high saltwater or other fluid flow through the formation resulting in fluid influx.

[0003] In a typical conductor pipe installation, a 60-77 cm (24-30 inch) outer diameter (OD) surface pipe is driven at least 61 m (200 feet) BML. A large diameter (60 cm (20 in.) OD when 77cm (30 in.) OD used) conductor pipe then is cemented by the conventional inner-string method through the drill pipe, with cement returns back to the ocean floor. Since no riser is used, the annular returns must be taken at the sea floor. Cool temperatures caused by the seawater typically slow the cement hydration process and extend the transition time of the cement slurry which allows fluid influx to begin. The term "transition time" refers to the period of time between the onset of hydration of the cement and the development of compressive strength wherein the gel strength increases to a level of about 240 Pa (500 lbf/100 ft²) whereby fluid migration is substantially prevented. During the transition time, a fluid such as oil, gas or water can migrate through the setting cement slurry forming channels that affect the integrity of the cement sheath. The fluid migration is possible during transition because the cement column in the well bore begins to support itself and stops exerting hydrostatic pressure on the fluid surrounding the well bore. When the exerted hydrostatic pressure falls below the formation fluid pressure, migration can occur and will continue until the cement develops sufficient compressive strength to prevent further migration.

[0004] In some instances, the formation sands may be over-pressured by water so that water or another formation fluid flows into the setting cement sheath during the transition time. Prevention of such flow is critical to a successful cementing job and to avoid expensive remedial squeeze cementing treatments. Containment of the over-pressured formation fluid often is complicated by weak zones in the formation that can fracture due to the fluid pressure of the cement slurry. If a fracture is

formed, the cement slurry can flow into the fracture and be lost from the well bore.

[0005] One method that has been utilized in the past has involved lightening the cement slurry by the addition of mix water. Such slurries have little useful strength at slurry densities below 1.3g/cm³ (11 lb/gal) and have long transition times because of the cool formation temperatures. Water-extending a cement slurry is accomplished by the addition of water and an extending material such as sodium silicate or bentonite to the normal cement slurry. The amount of water-extending material and water added to the normal weight cement slurry depends on the final desired cement slurry density and the requirement of little or no free water in the cement slurry.

[0006] The use of water-extended cement slurries in deepwater completions has resulted in numerous well problems due to the cemented annulus being highly contaminated by formation fluids whereby the cement sheath can not adequately support the conductor string. This can result in casing buckling and loss of the well.

[0007] We have now devised a method by which a cementing operation can be performed on a conductor casing in over-pressured, poorly consolidated formations. We have also found a way to shorten the transition time of the cement while making the drilling mud and cement slurry weight compatible with the formation fracture gradients to avoid cement losses to the formation.

[0008] According to the present invention, there is provided a method of cementing a conductor pipe in an underwater well bore, which method comprises flowing a cementing slurry through the conductor pipe and returning it from the lower end of the pipe through an annulus between the pipe and the well bore; and maintaining the slurry in the annulus for a sufficient time to enable the slurry to form a rigid cement sheath in the annulus; wherein the cementing slurry comprises a Portland cement having a Blaine Fineness less than 3900 cm²/gm, from 1 to 30 percent by weight of said Portland cement being a fine particle size cementitious material having a Blaine Fineness of no less than 6000 cm²/gm and having a particle size no greater than 30 micrometres (microns), the slurry containing from 0.4 to 0.85 weight parts of aqueous fluid per weight part of said Portland cement, and from 1 to 10 percent, by volume of the aqueous fluid, of a foaming surfactant, and sufficient gas to foam the slurry.

[0009] Preferably the method is carried out in a water depth of at least 305m.

[0010] In the method of the invention, the cement slurry preferably has a density of from about 1.0 to about 1.7g/cm³ (9.0 to about 14 lbs/U.S.gal.) The slurry is formulated to provide a transition time of from about 30 minutes or less at the temperature of the sea floor. The presence of the nitrogen or other gas in the slurry aids in controlling the slurry density and facilitates maintenance of the pressure gradient in the well bore during

the transition time of the cement below the fracture gradient.

[0011] US-A-5133409 describes a method of cementing a well penetrating a salt containing subterranean formation using a foamed cement composition comprising Portland cement, gas, a foaming agent and a foam stabiliser. The compositions do not use fine particle Portland cement nor are they described for use in cementing conductor pipes in underwater formations.

[0012] In order that the invention may be more fully understood, embodiments thereof will now be described by way of example only with reference to the accompanying drawings, in which:

Figure 1 is a diagrammatic schematic illustration of a deepwater cementing in soft formations such as beyond the continental shelf; and

Figure 2 is a schematic illustration of a portion of a conductor casing cemented in a soft formation subject to water influx.

[0013] The present invention provides a method for successfully cementing the conductor pipe in offshore operations in water depths for example in excess of 305m (100 feet) and where the mud and near sea floor formations are poorly consolidated or unstable.

[0014] Figure 1 provides a diagrammatic illustration of the cementing of a deepwater well in accordance with the prior art techniques described hereinbefore. A drilling platform 10 has positioned a surface pipe 12 through the mudline layer 20 and a conductor pipe 14 into the formation 22 in the seafloor. A conventional cement slurry is pumped through a string 16 and associated packers into the conductor pipe 14 and cement returns are taken at the seafloor 18. Figure 2 provides a diagrammatic illustration of the problem created by the influx of undesired fluid into the cement slurry during the transition time of the cement slurry. The flow of water or other fluid into the slurry from water zones 24 in formation 22 creates undesired passages 26 in the cement which effects the integrity of the cement bond with the conductor pipe.

[0015] The method of the present invention prevents the undesired influx of fluid into the well bore. In accordance with the method of the present invention, the conductor casing is positioned within the well bore and the drilling mud present in the well bore is displaced and substantially removed from the face of the well bore by circulation of a spacer fluid. Such fluids are well known to those individuals skilled in the art of cementing well bores in subterranean formations, therefore no specific method of formulation of such a fluid is considered necessary.

[0016] In a preferred embodiment, the drilling mud utilized would have the following general properties: API fluid loss of less than about 7 cc/30 minutes, a yield point of about 9 Pa (20 lbf/100 ft²) a plastic viscosity of about 15 cp and a generally flat gel strength develop-

ment over time. The drilling fluid preferably is displaced with turbulent flow of a conventional high viscosity spacer fluid. Preferably the spacer fluid has a minimum of 10 minutes contact time with the drilling mud filter cake in the well bore.

[0017] The cement slurry of the present inventions then is introduced into the conductor pipe. The conductor pipe is generally of a length of from about 150m to about 765 m (about 500 to about 2500 feet) when utilized in deepwater completions. The slurry is introduced in sufficient volume to fill the annulus from the base of the well bore to the surface of the sea floor. Generally, a volume of 1.2 to 1.5 times the estimated annular volume will be utilized to assure sufficient return to the sea floor.

The slurry comprises a quantity of hydraulic cement such as, for example, Portland class A, C, G or H. The average particle size of such cement is typically in excess of 80 micrometres (microns). The particle size of the cement can also be indirectly expressed in terms of surface area per unit weight of a given sample of material. This value, sometimes referred to as the Blaine Fineness or as specific surface area, can be expressed in the units square centimetres per gram (cm²/gm). The Blaine Fineness of conventional hydraulic cement is less than about 3900 cm²/gm. To the conventional hydraulic cement is added from about 1 to about 30 percent by weight of conventional cement of a cementitious material having particle diameters no larger than about 30 micrometres (microns), preferably no larger than about 17 micrometres (microns), and still more preferably no larger than about 11 micrometres (microns). The distribution of various sized particles within the cementitious material, i.e., the particle size distribution, features 90 percent of them having a diameter not greater than about 25 micrometres (microns), preferably about 10 micrometres (microns) and still more preferably about 7 micrometres (microns). Fifty (50) percent having a diameter not greater than about 10 micrometres (microns), preferably about 6 micrometres (microns) and still more preferably about 4 micrometres (microns) and 20 percent of the particles having a diameter not greater than about 5 micrometres (microns) preferably about 3 micrometres (microns) and still more preferably about 2 micrometres (microns).

[0018] The Blaine Fineness of the fine particle size cementitious material used in the cementing methods of this invention is no less than about 6000 cm²/gram. The value is preferably greater than about 7000, more preferably about 10,000, and still more preferably greater than about 13,000 cm²/gram.

[0019] Cementitious materials of particle size and fineness as set out above are disclosed in various prior U.S. Patent numbers including Clark, U.S. Patent No. 4,761,183, which is drawn to slag, as defined herein, and mixtures thereof with ultrafine Portland cement, and Sawyer, U.S. Patent No. 4,160,674 which is also drawn to Portland cement. The fine particle size cementitious materials preferred for use in this invention are ultrafine

Portland cement and combinations thereof with slag wherein the quantity of Portland cement included in any mixture of Portland cement and slag used in the methods of this invention can be as low as 10 percent but is preferably no less than about 40 percent, more preferably about 80 percent and most preferably no less than about 100 percent Portland cement by weight of mixture. The fine particle size cementitious material is more fully described in U.S. Patent No. 5,125,455, to which reference should be made for further details.

[0020] The cementitious material is formulated into an aqueous slurry by admixture with an aqueous fluid such as fresh water, seawater or substantially any other aqueous fluid. The slurry may be formulated utilizing ratios of the weight of water per unit weight of conventional cement material in the range of a from about 0.4 to about 0.85 and preferably from about 0.55 to about 0.65 pounds per pound of conventional cement material.

[0021] When fresh water is utilized to formulate the slurry, a foaming surfactant such as an anionic ethoxylated $C_8 - C_{15}$ linear alcohol sulfonate may be admixed with the slurry together with a stabilizer such as, for example, a capped polyethylene oxide such as "CARED WAX" foam stabilizer, a product of Union Carbide. The surfactant may be present in an amount of from about 1 to about 10 percent by volume of water utilized in the slurry preferably from about 1 to about 5 percent by volume of water and most preferably about 3 percent by volume of water. The stabilizer may be present in an amount of from about 0.25 to about 2 percent by volume of water utilized in the slurry and preferably about 0.75 percent by volume of water.

[0022] Alternatively, any other known surfactant or surfactant and stabilizer which will function to form a stable foam in cement/fresh water slurries may be utilized.

[0023] When seawater is utilized to formulate the slurry a foaming surfactant such as an amphoteric fatty amine such as a betaine of coco-amine may be admixed with the slurry and a stabilizer such as, for example, a salt of an alkyl ether sulfate may be included. The surfactant and stabilizer may be present in the same ranges as for fresh water. Preferably, the surfactant is present in the seawater slurry in an amount of from about 3 to 4 percent by volume of seawater and the stabilizer is present in an amount of about 0.75 percent by volume of seawater.

[0024] Alternatively any other surfactant or surfactant/stabilizer mixture may be employed which is capable of stabilizing the foamed cement slurry.

[0025] The slurry is foamed by the addition of nitrogen or other gas to the mixture of cement, aqueous fluid, surfactant and stabilizer. The density of the slurry may be controlled by the amount of nitrogen gas admixed with the slurry. The slurry density can be adjusted to any desired level within a range of from about 1.0 to about 1.7g/cm^3 (9 to about 14 pounds per gallon) by the addi-

tion of from about 8.4m^3 to as little as 2.8m^3 (300 to as little as 100 standard cubic feet (SCF)) of nitrogen gas at standard conditions per barrel of unfoamed cement slurry. The specific density of the cement slurry will depend upon several factors, however, it is important to maintain the density at a level such that the fracturing gradient of the near surface formation in which the conductor pipe is being cemented is not exceeded. Generally, the density will be adjusted to provide a level slightly above the formation pressure but below the fracturing gradient to maintain control over the slurry and prevent fluid influx during the transition time of the cement slurry. Preferably, the density will be adjusted to a level of about 0.1g/cm^3 (1 lb/gal) above the density required to match the formation pressure in the well bore.

[0026] The cement slurry also may contain other conventional additives such as accelerators, fluid-loss control agents, additives to control free water or solids separation and the like, silica fume, glass or ceramic micropheres, perlite and the like.

[0027] The slurry upon placement in the well bore rapidly develops sufficient compressive strength to prevent the influx of formation fluids before loss of the hydrostatic pressure control effected by the nitrogen or gas foam during the transition time when the slurry is static. The slurry develops a gel strength (yield point) in excess of about 240 Pa (500 lbf/100 ft²) within about 30 minutes of the time of placement which substantially prevents fluid migration through the cement sheath in the well bore. This is in contrast to conventional cement slurries which may take 3 to 6 hours or more to develop a similar yield point and which permit fluid influx as a result.

[0028] To further illustrate the present invention, while not intended or considered to limit the present invention, the following example is provided.

[0029] A well bore is completed in the Gulf of Mexico in 824m (2700 feet) of water. A 51 cm (20 inch) conductor pipe is positioned in a 66cm (26 inch) well bore. The length of the conductor pipe is 549m (1800 feet). The cement slurry is designed to provide a 25% volumetric excess to ensure return to the seafloor. The slurry is comprised of 1620 sacks of class A Portland cement, 3418m^3 (122081 SCF) of nitrogen gas, 12462 kg (27450 pounds) of fine particle size cementitious material, 863 kg (1900 pounds) of calcium chloride, 1440 litres (380 gallons) of a surfactant comprising a betaine of a coco-amine, and 364 litres (96 gallons) of an alkyl ether sulfate stabilizer. The aqueous fluid admixed with the cement to form the slurry is seawater and the seawater is admixed with the cement in an amount of 25.8 litres (6.8 gallons) per sack of conventional Portland cement. The fluid is pumped through drill pipe to the conductor casing and permitted to return up the annulus to the seafloor. The cement exhibited a transition time of less than 30 minutes and no formation fluid influx is found to occur.

[0030] While that which is considered to be the pre-

ferred embodiment of the present invention has been described herein, it is to be understood that other embodiments have been suggested and still others will occur to those skilled in the art upon a reading and understanding of the foregoing specification. It is intended that all such embodiments be included within the scope of this invention.

Claims

1. A method of cementing a conductor pipe in an underwater well bore, which method comprises flowing a cementing slurry through the conductor pipe and returning it from the lower end of the pipe through an annulus between the pipe and the well bore; and maintaining the slurry in the annulus for a sufficient time to enable the slurry to form a rigid cement sheath in the annulus; wherein the cementing slurry comprises a Portland cement having a Blaine Fineness less than 3900 cm²/gm, from 1 to 30 percent by weight of said Portland cement being a fine particle size cementitious material having a Blaine Fineness of no less than 6000 cm²/gm and having a particle size no greater than 30 micrometres (microns); the slurry containing from 0.4 to 0.85 weight parts of aqueous fluid per weight part of said Portland cement, and from 1 to 10 percent, by volume of the aqueous fluid, of a foaming surfactant, and sufficient gas to foam the slurry.
2. A method according to claim 1, wherein nitrogen gas is mixed with the cement slurry to provide a slurry with a density of from 1.0 to 1.7 g/cm³ (9 to 14 pounds per U.S. gallon).
3. A method according to claim 1 or 2, wherein the nitrogen gas is mixed with said cement slurry in an amount of from 2.8 to 8.4 m³ (100 to 300 SCF) per barrel of unfoamed cement slurry.
4. A method according to claim 1, 2 or 3, wherein the slurry develops a yield point in excess of 240 Pa (500 lb/100 ft²) in the annulus in less than 30 minutes.
5. A method according to claim 1, 2, 3 or 4, wherein the surfactant is present in an amount of from 1 to 5 percent by volume of the aqueous fluid.
6. A method according to any of claims 1 to 5, wherein the cement slurry includes a foam stabilizer in an amount of from 0.25 to 2 percent by volume of the aqueous fluid.
7. A method according to claim 6, wherein the stabilizer comprises a capped polyethylene oxide or a salt of an alkyl ether sulfate, or any mixture of two or more thereof.

8. A method according to any of claims 1 to 7, wherein the foaming surfactant comprises an amphoteric fatty amine or an anionic ethoxylated C₈ - C₁₅ linear alcohol sulfonate, or any mixture of two or more thereof.
9. A method according to any of claims 1 to 8, wherein the maximum particle size of the fine cementitious material is 11 micrometres (microns) and the Blaine Fineness is no less than 10,000 cm²/gm.
10. A method according to any of claims 1 to 9, wherein said cement slurry includes an accelerator comprising calcium chloride.

Patentansprüche

1. Eine Vorgehensweise des Zementierens eines Förderrohres in einem unter einer Wasserschicht ausgeführten Bohrloch, bestehend aus den folgenden Schritten: Einströmen eines Zementschlammes durch das Förderrohr und Rückspülen des Schlammes durch den Ringraum zwischen dem Rohr und dem Bohrloch sowie ausreichend langem Halten des Schlammes im Ringraum, damit sich der Schlamm zu einem starren Zementmantel im Ringraum entwickeln kann, wobei der Zementschlamm einen Portlandzement mit Blainescher Feinheit unter 3900 cm²/g aufweist und von 1 bis 30 Gew.% des erwähnten Portlandzements einen zementösen Stoff mit feiner Partikelgröße und Blainescher Feinheit von mindestens 6000 cm²/g aufweist, während seine Partikelgröße höchstens 30 µm ist. Der Schlamm enthält den erwähnten Portlandzement in Gewichtsanteilen der wässrigen Flüssigkeit von 0,4 bis 0,85 pro Gewichtsanteil und ein schäumendes Tensid von 1 bis 10 Vol. Prozent der wässrigen Flüssigkeit sowie ausreichend Gas, um den Schlamm zu schäumen.
2. Eine Vorgehensweise nach Anspruch 1, bei der das Stickstoffgas mit dem Zementschlamm vermischt wird, um einen Schlamm mit einer Dichte von 1,0 bis 1,7 g/cm³ zu bilden.
3. Eine Vorgehensweise nach Ansprüchen 1 oder 2, bei der das Stickstoffgas im Verhältnis von 2,8 bis 8,4 m³ pro Faß ungeschäumten Zementschlammes mit diesem vermischt wird.
4. Eine Vorgehensweise nach Ansprüchen 1, 2 oder 3, wobei der Schlamm im Ringraum in weniger als 30 Minuten eine Fließgrenze über 240 Pa entwickelt.
5. Eine Vorgehensweise nach einem der Ansprüche 1, 2, 3 oder 4, bei der das Tensid im Verhältnis von 1 bis 5 Prozent der wässrigen Flüssigkeit vorhan-

den ist.

6. Eine Vorgehensweise nach einem der Ansprüche 1 bis 5, wobei der Zementschlamm einen Schaumstabilisator im Verhältnis von 0,25 bis 2 Vol Prozent der wässrigen Flüssigkeit enthält. 5
7. Eine Vorgehensweise nach Anspruch 6, wobei der Stabilisator ein gekapptes PE-Oxid oder Salz eines Alkylethersulfats oder eine Mischung beider umfaßt. 10
8. Eine Vorgehensweise nach einem der Ansprüche 1 bis 7, wobei das schäumende Tensid ein amphoteres Fettamin oder ein lineares anionisches ethoxyliertes C₈ - C₁₅ Alkoholsulfonat oder eine Mischung beider umfaßt. 15
9. Eine Vorgehensweise nach einem der Ansprüche 1 bis 8, bei der die maximale Partikelgröße des feinen zementösen Stoffes 11 µm und die Blainesche Feinheit mindestens 10 000 cm²/g ist. 20
10. Eine Vorgehensweise nach einem der Ansprüche 1 bis 9, wobei der erwähnte Zementschlamm ein Beschleunigungsmittel aus Chlorkalzium enthält. 25

Revendications

1. Un procédé de cimentation d'un tube guide dans un trou de forage sous-marin, ledit procédé comportant l'écoulement d'un laitier de cimentation à travers le tube guide et son renvoi à partir de l'extrémité inférieure du tube à travers un espace annulaire entre le tube et le trou de forage ; et le maintien du laitier dans l'espace annulaire pendant une durée suffisante pour permettre au laitier de former une gaine de ciment rigide dans l'espace annulaire ; selon lequel le laitier de ciment comprend un ciment Portland ayant une finesse Blaine de moins de 3900 cm²/gm, de 1 à 30 pour cent en poids dudit ciment Portland étant une matière cimenteuse à granulométrie fine ayant une finesse Blaine minimum de 6000 cm²/gm et ayant une granulométrie minimum de 30 micromètres (microns), le laitier contenant de 0,4 à 0,85 parties en poids de fluide aqueux par partie en poids dudit ciment Portland, et de 1 à 10 pour cent, par volume du fluide aqueux, d'un surfactant moussant, et une quantité de gaz suffisante pour faire mousser le laitier. 30 35 40 45 50
2. Un procédé selon la revendication 1, selon lequel l'azote en phase gazeuse est mélangé avec le laitier de ciment pour produire un laitier d'une densité de 1,0 à 1,7 g/cm³ (9 à 14 pounds/livres par gallon U.S.). 55
3. Un procédé selon la revendication 1 ou 2, selon

lequel l'azote en phase gazeuse est mélangé avec ledit laitier de ciment en une quantité de 2,8 à 8,4 m³ (100 à 300 SCF) par baril de laitier de ciment non moussé.

4. Un procédé selon la revendication 1, 2 ou 3, selon lequel le laitier développe un seuil de plasticité excédant 240 Pa (500 lb/100ft²) dans l'espace annulaire en moins de 30 minutes.
5. Un procédé selon la revendication 1, 2, 3 ou 4, selon lequel le surfactant est présent en une quantité de 1 à 5 pour cent par volume du fluide aqueux.
6. Un procédé selon l'une quelconque des revendications 1 à 5, selon lequel le laitier de ciment inclut un stabilisateur de mousse en une quantité de 0,25 à 2 pour cent par volume de fluide aqueux.
7. Un procédé selon la revendication 6, selon lequel le stabilisateur comporte un oxyde de polyéthylène capped ou un sel d'un sulfate d'éther alkyle, ou un mélange quelconque de deux de ceux-ci ou davantage.
8. Un procédé selon l'une quelconque des revendications 1 à 7, selon lequel le surfactant mousseux comprend un amine gras amphotérique ou un sulfonate d'alcool linéaire C₈ - C₁₅ anionique éthoxylé, ou un mélange quelconque de deux de ceux-ci ou davantage.
9. Un procédé selon l'une quelconque des revendications 1 à 8, selon lequel la granulométrie maximale du matériau cimenteux fin est de 11 micromètres (microns) et la finesse Blaine n'est pas inférieure à 10.000 cm²/gm.
10. Un procédé selon l'une quelconque des revendications 1 à 9, selon lequel ledit laitier de ciment inclut un accélérateur comportant du chlorure de calcium.

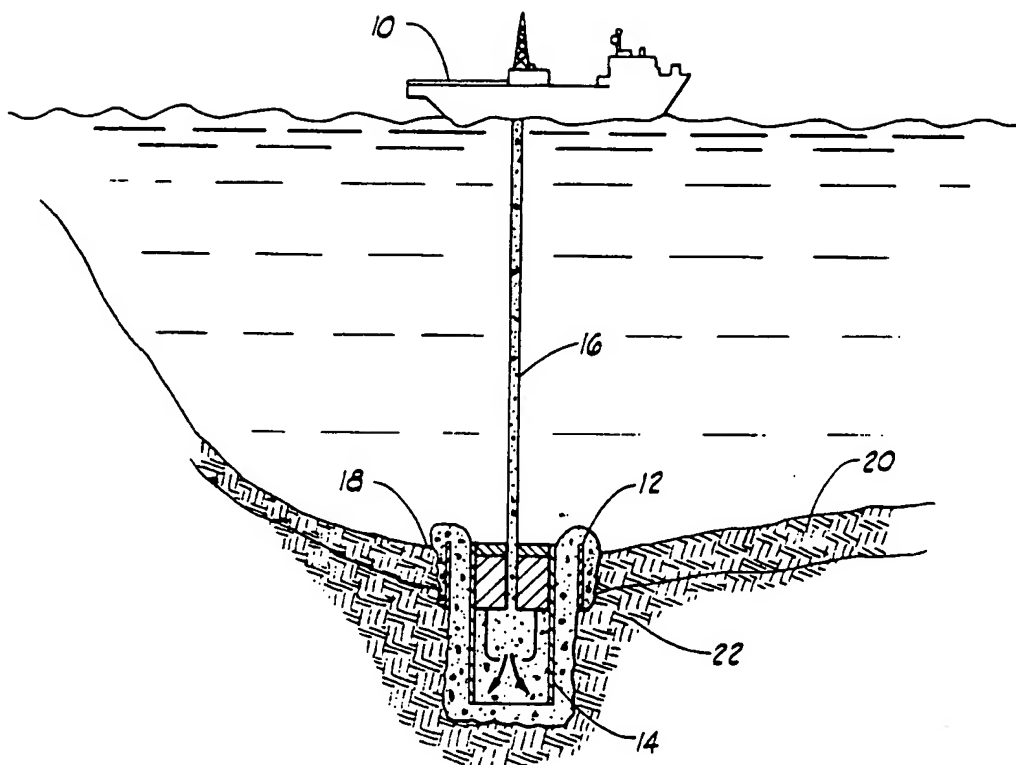


FIG. 1

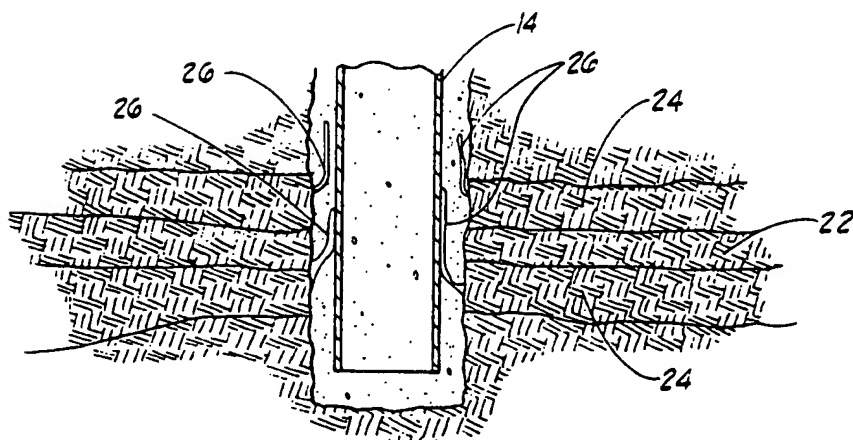


FIG. 2

THIS PAGE BLANK (USPTO)